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Dipartimento di Ingegneria Chimica,  
Gestionale, Informatica, Meccanica (DICGIM)



# *Performance analysis of the first Reverse Electrodialysis prototype plant operating with natural brackish water and saltworks brine*

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2<sup>nd</sup> International Conference on Salinity Gradient Energy  
Leeuwarden, The Netherlands, 10-12 September 2014

# Outline

## 1. Introduction

- The use of natural solutions for RED process
- The REAPower prototype plant

## 2. Plant design and construction

- Process Flow Diagram
- Piping layout
- Equipment and Instrumentation
- Pre-treatment of concentrate and dilute solutions

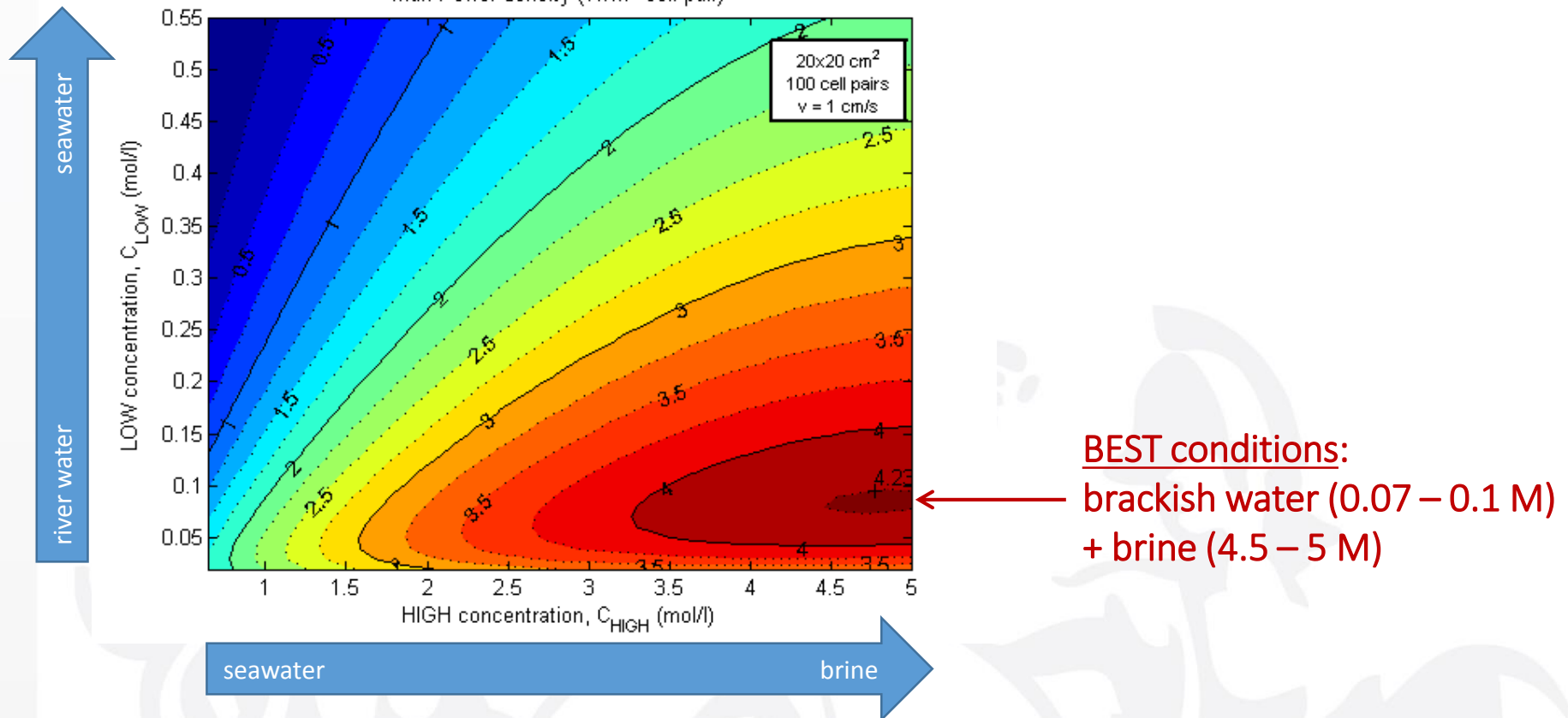
## 3. Installation and start-up

- Installation of the first prototype and start-up
- scale-up

## 4. Results and Perspectives

- Power measurements with natural solutions
- Power measurements with artificial solutions

# The use of natural solutions for RED process



**BEST conditions:**  
brackish water (0.07 – 0.1 M)  
+ brine (4.5 – 5 M)

Simulations of a **20x20 cm<sup>2</sup>** stack (**100-cells**) equipped with Fujifilm membranes, 270  $\mu\text{m}$  spacers; feed flow velocity: 1 cm/s; T=20°C.

# The REAPower prototype plant

## Facts and figures:



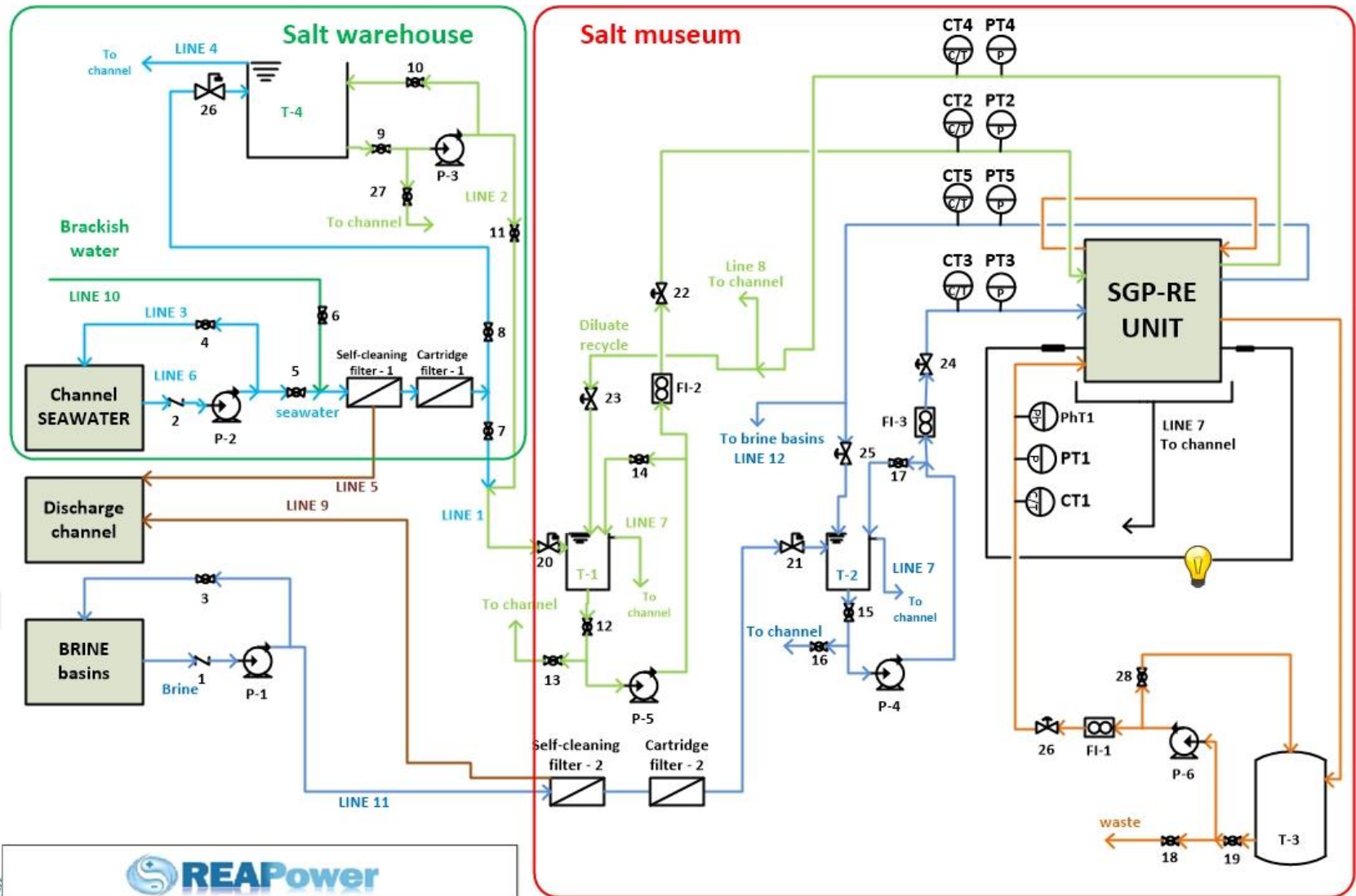
- ✓ **Saline solutions** available on site:
  - saturated brine (conductivity: 200 mS/cm,  $\approx$  250-300 g/l)
  - brackish water (conductivity: 3.4 mS/cm,  $\approx$  2 g/l)
  - seawater
  
- ✓ High **feed solution temperature** during summer (30°C)
  
- ✓ Use of **Iron Chloride** ( $\text{FeCl}_2/\text{FeCl}_3$ ) as electrode rinse solution



**Trapani saltworks  
(Sicily, South of Italy)**

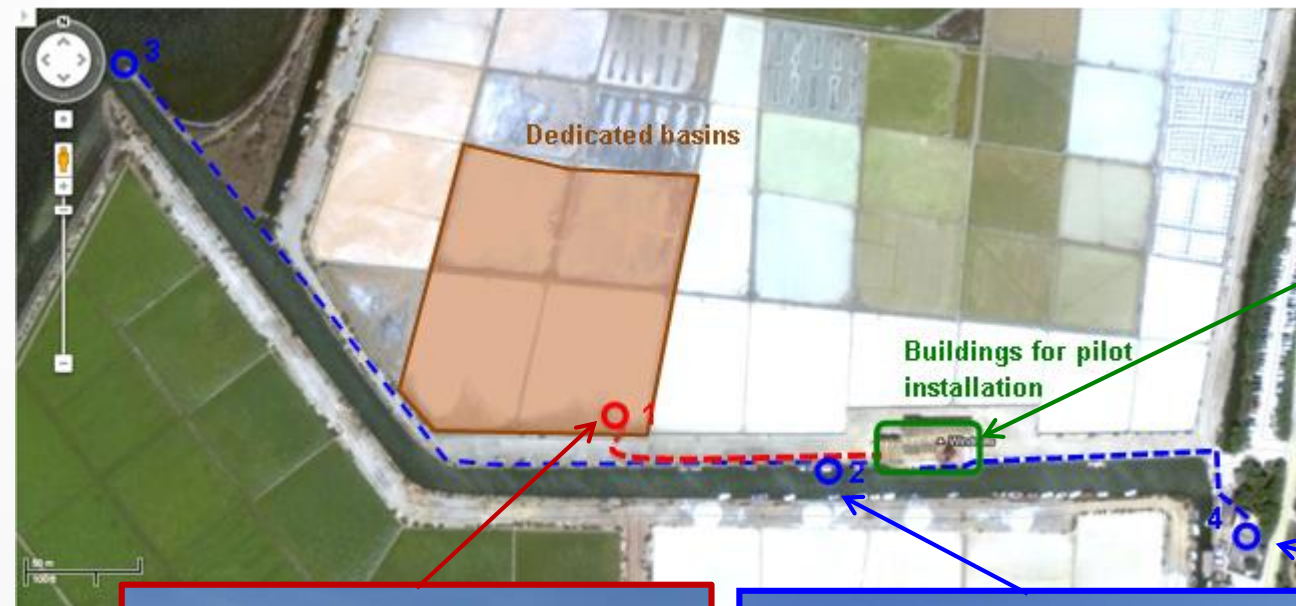


# Process flow diagram



Scalici Claudio	WP7 Pilot Prototype
Installation site: Ettore-Infersa saltworks	28/05/2014

# Piping layout



brine intake



seawater intake

Brackish water well



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# Equipment and Instrumentation

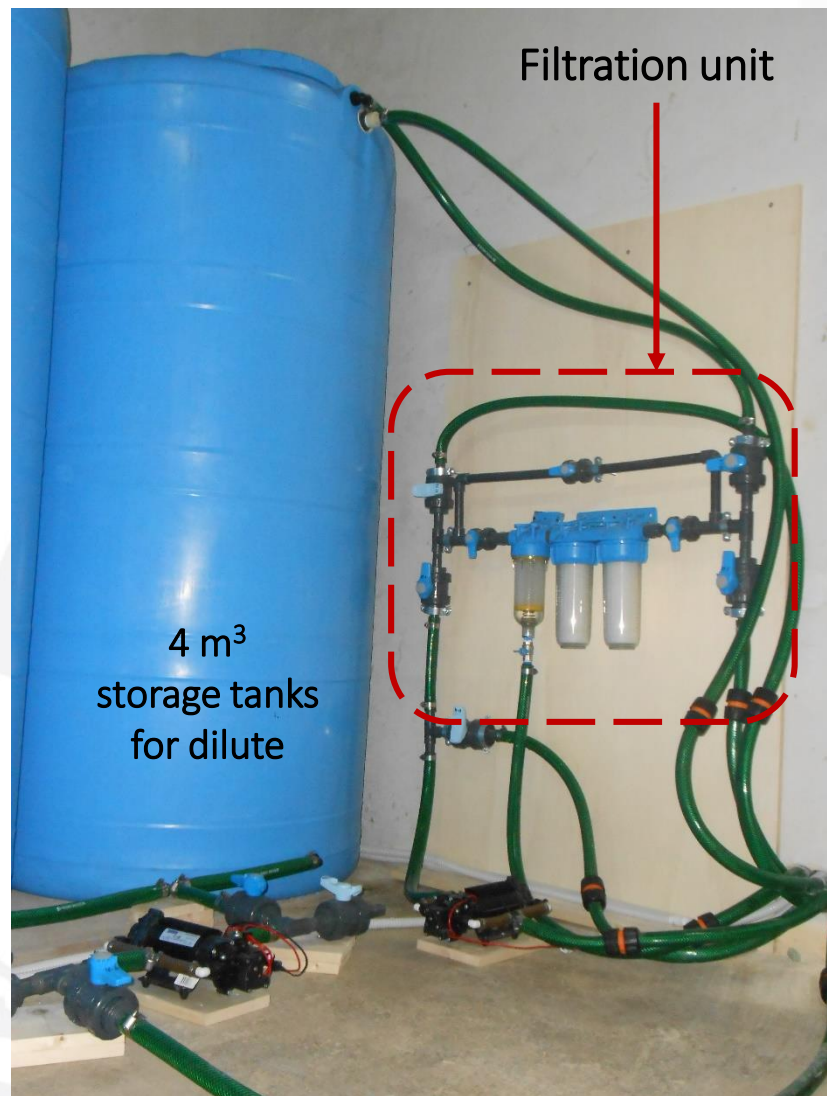
Measuring devices for:

- Pressure
- Conductivity/  
Temperature
- Flow rate



# Pre-treatment of concentrate and dilute solutions

SELF-CLEANING  
FILTER  
50 micron    +    FILTER  
25 micron    +    FILTER  
5 micron

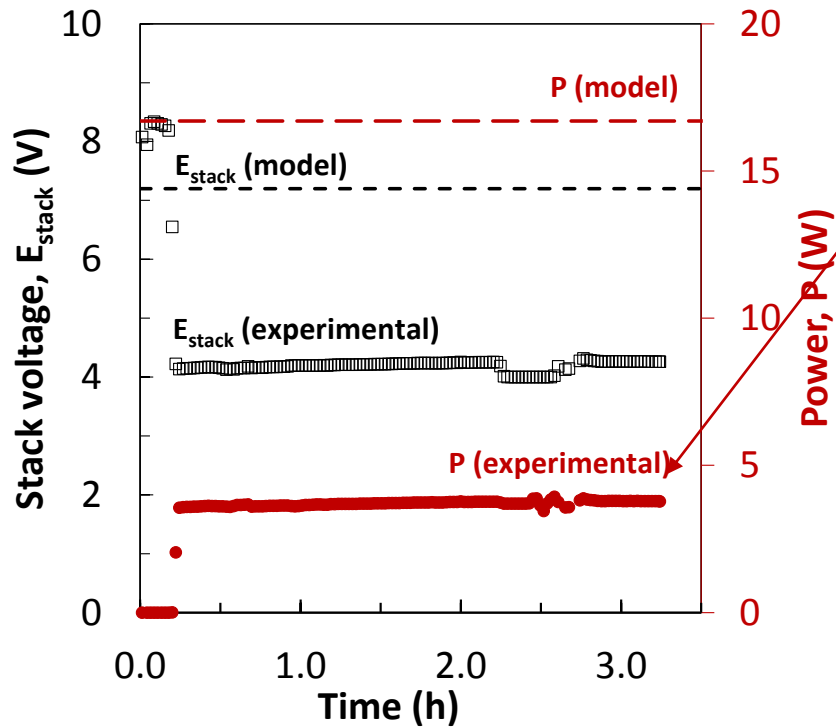


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- SGE Conference 2014



# Installation of the first prototype and start-up

(22x22 cm<sup>2</sup> stack, 109 cell pairs)



**Low power production due to:**

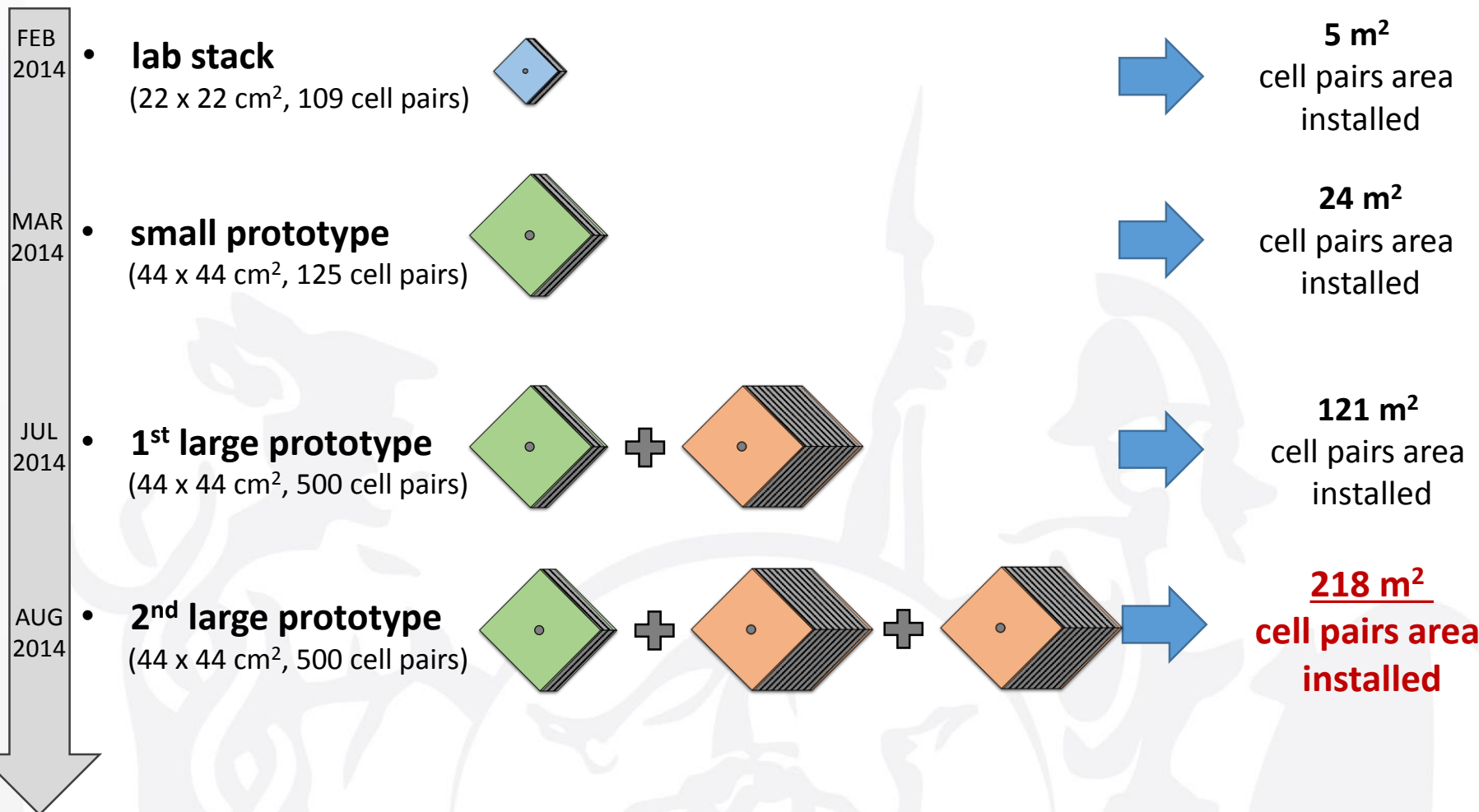
- non-optimal membranes (designed for river water/ seawater)
- diluted brine ( $\approx 2$  M NaCl).

22x22 cm<sup>2</sup> 109 cell pairs stack fed with **brackish water (3.4 mS/cm)** and **brine (137 mS/cm)**.  
 T = 17°C. Flow rate: 6 l/min (1 cm/s).

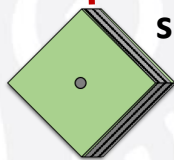


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# Plant scale-up

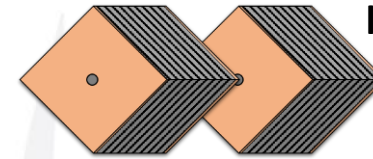


# Plant scale-up: final configuration



**small prototype**

44 x 44 cm<sup>2</sup>  
125 cell pairs



**large prototypes**

44 x 44 cm<sup>2</sup>  
500 cell pairs

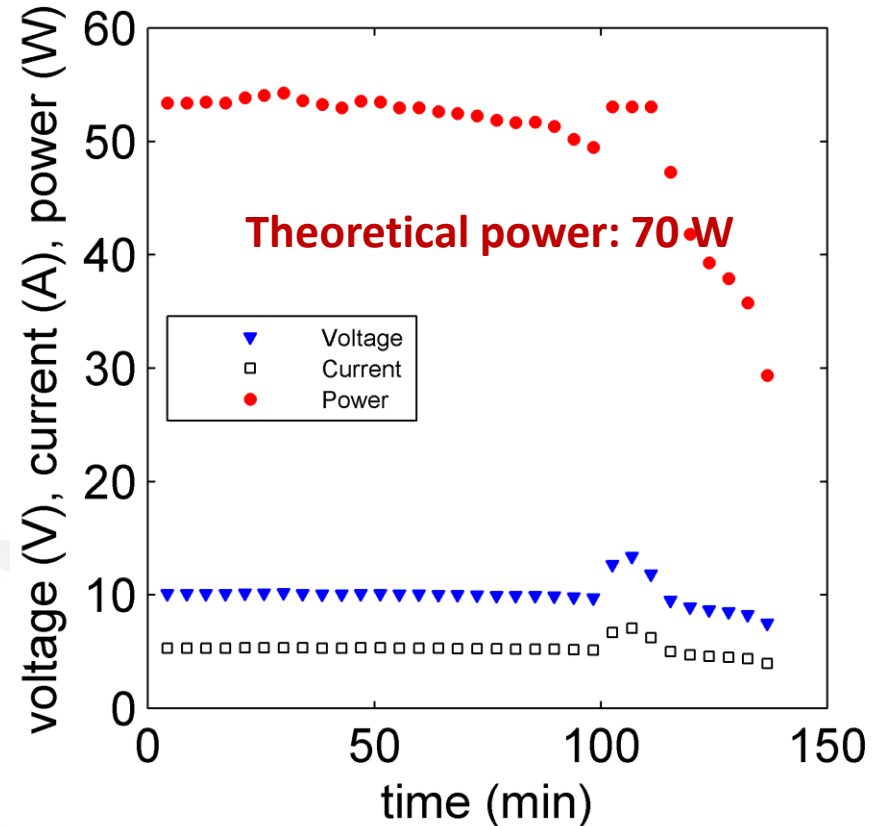
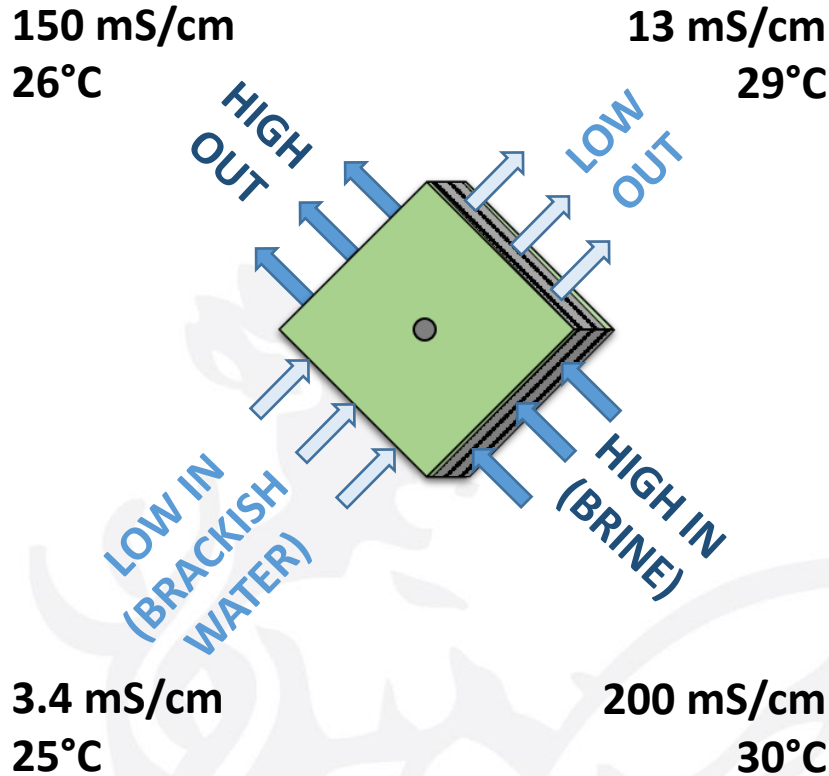


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# Power measurements with **natural** solutions (1/4)

Standard test conditions (1 cm/s velocity)

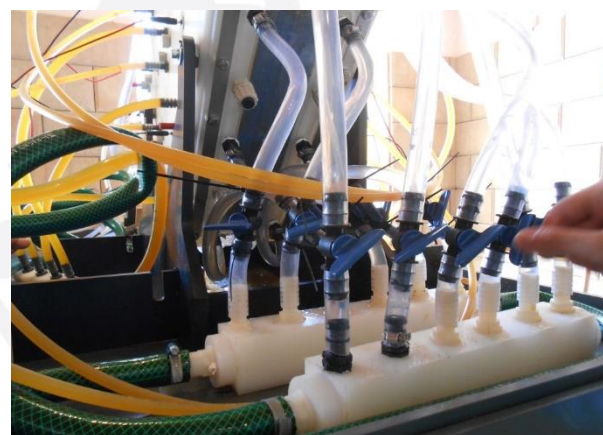
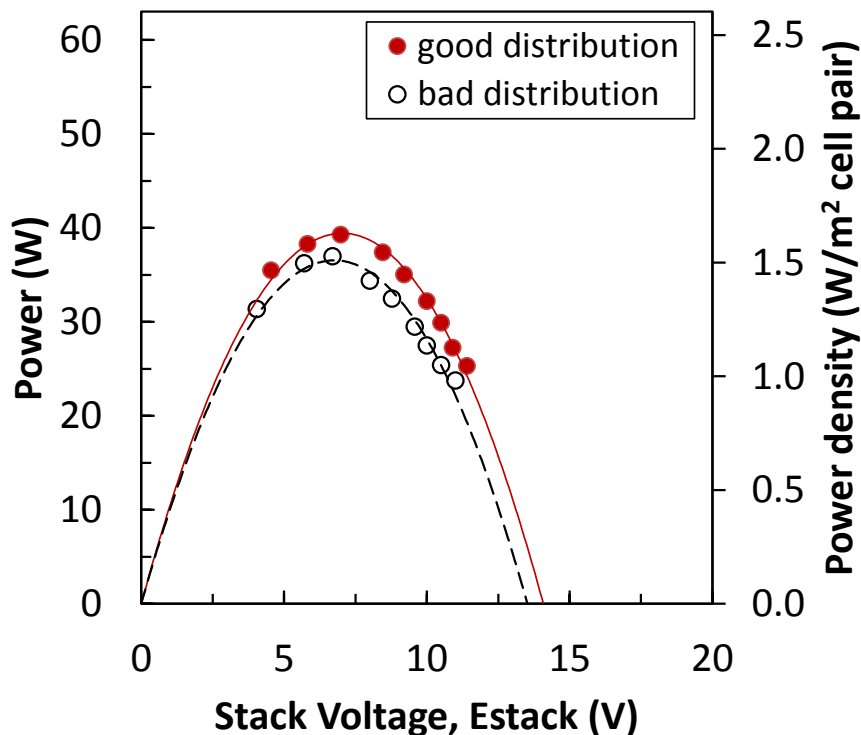


44x44 cm<sup>2</sup> 125 cell pairs stack fed with brackish water and saturated brine. Feed flow rate: **8 l/min** (1 cm/s).  
 $R_{load} = 1.9 \text{ ohm}$ .



# Power measurements with natural solutions (2/4)

## Influence of flow distribution on power output



First test (○): standard conditions (flow rates: 8 l/min).

Second test (●): improving the flow rate distribution by the inlet-outlet plugs. 44x44 cm<sup>2</sup> 125 cell pairs stack fed with brackish water (3.4 mS/cm) and brine (**170 mS/cm**).



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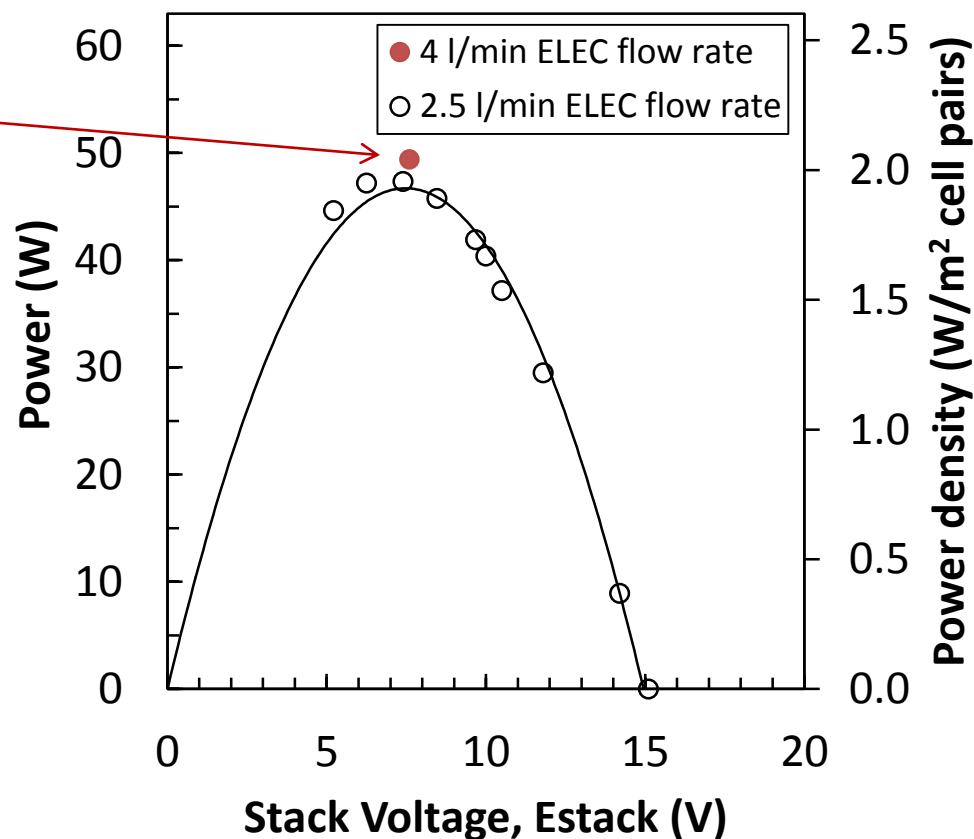
# Power measurements with **natural** solutions (3/4)

## Influence of electrode solution flow rate

Increasing electrode  
solution flow rate  
(4 l/min)

### ELECTRODE SOLUTION:

- 0.1 M  $\text{FeCl}_2$
- 0.1 M  $\text{FeCl}_3$
- 2.5 M NaCl



44x44 cm<sup>2</sup> 125 cell pairs stack fed with brackish water (3.4 mS/cm) and brine (200 mS/cm).

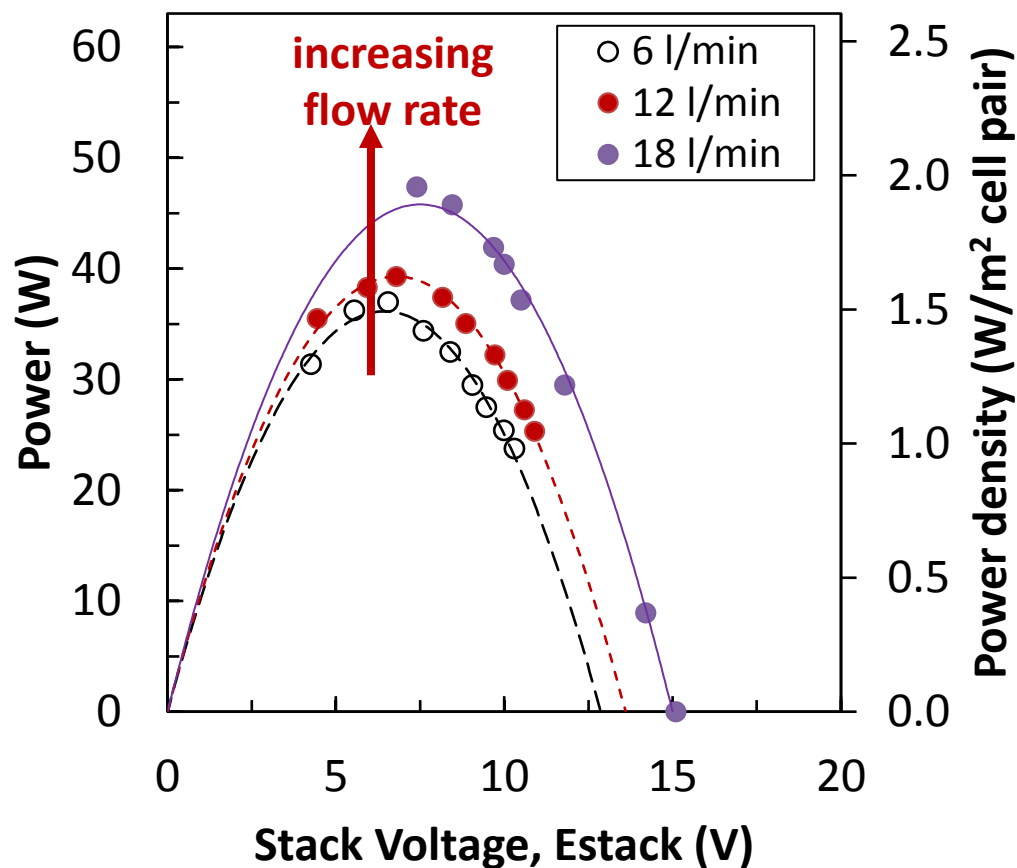


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# Power measurements with **natural** solutions (4/4)

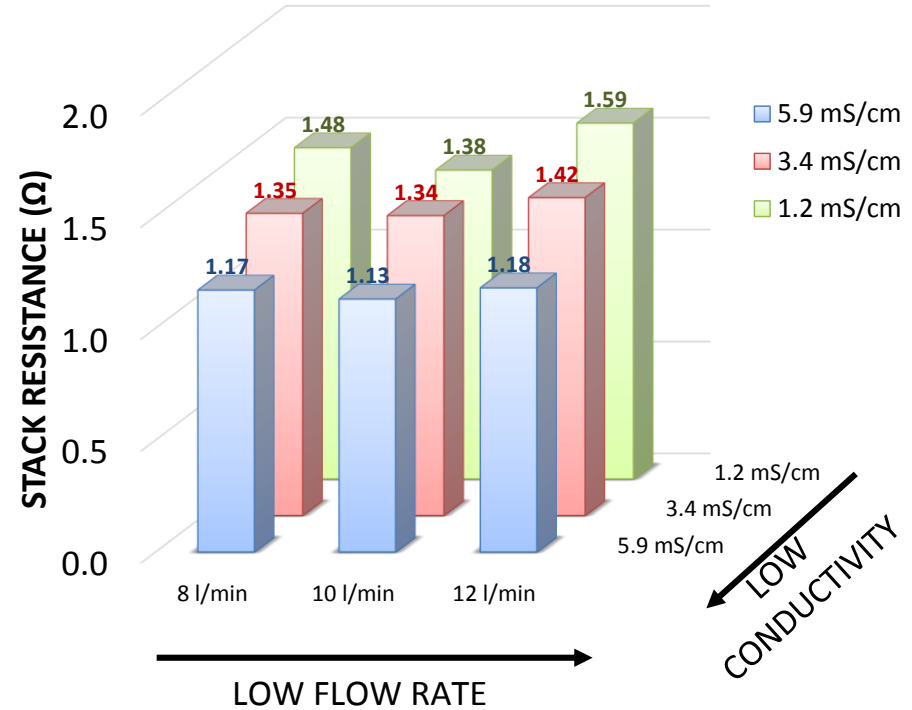
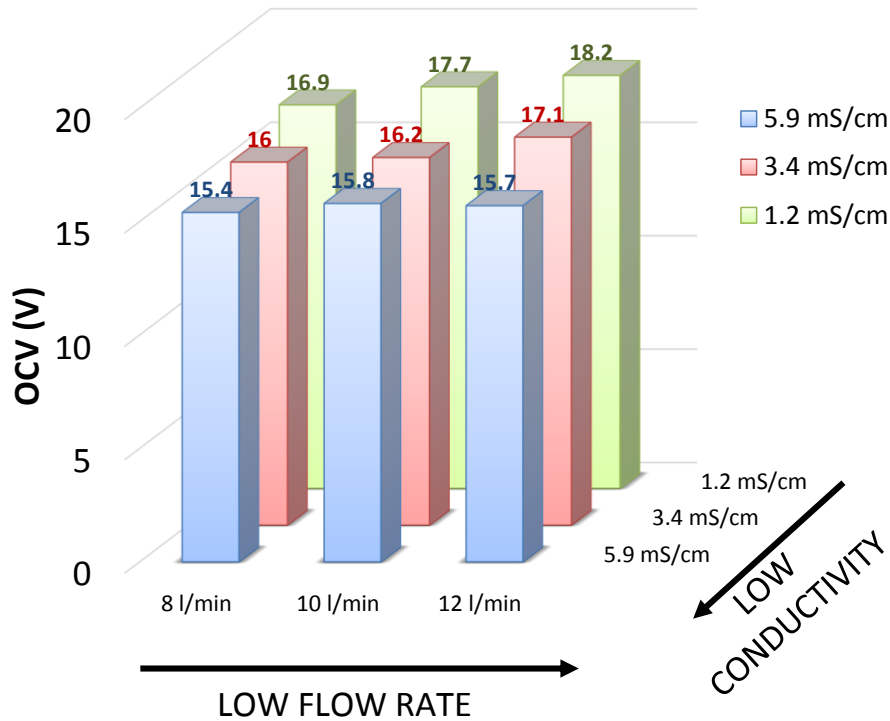
## Influence of dilute flow rate



44x44 cm<sup>2</sup> 125 cell pairs stack fed with brackish water (3.4 mS/cm) and brine (200 mS/cm).

# Power measurements with artificial solutions (1/3)

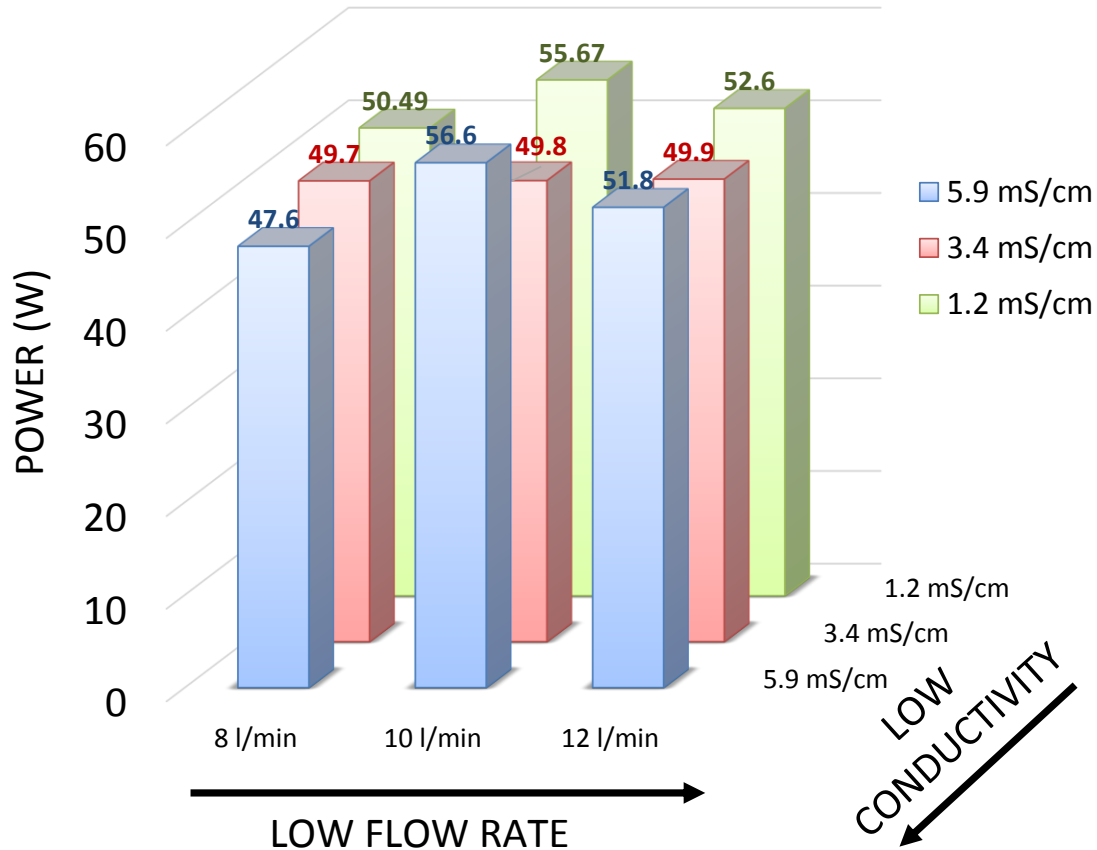
## Influence of dilute conditions on OCV and stack resistance



44x44 cm<sup>2</sup> 125 cell pairs stack fed with **artificial brine (215 mS/cm)** and **artificial brackish water (1.2 – 5.9 mS/cm)**.

# Power measurements with artificial solutions (2/3)

## Influence of dilute conditions on power output



44x44 cm<sup>2</sup> 125 cell pairs stack fed with **artificial brine (215 mS/cm)** and **artificial brackish water (1.2 – 5.9 mS/cm)**.

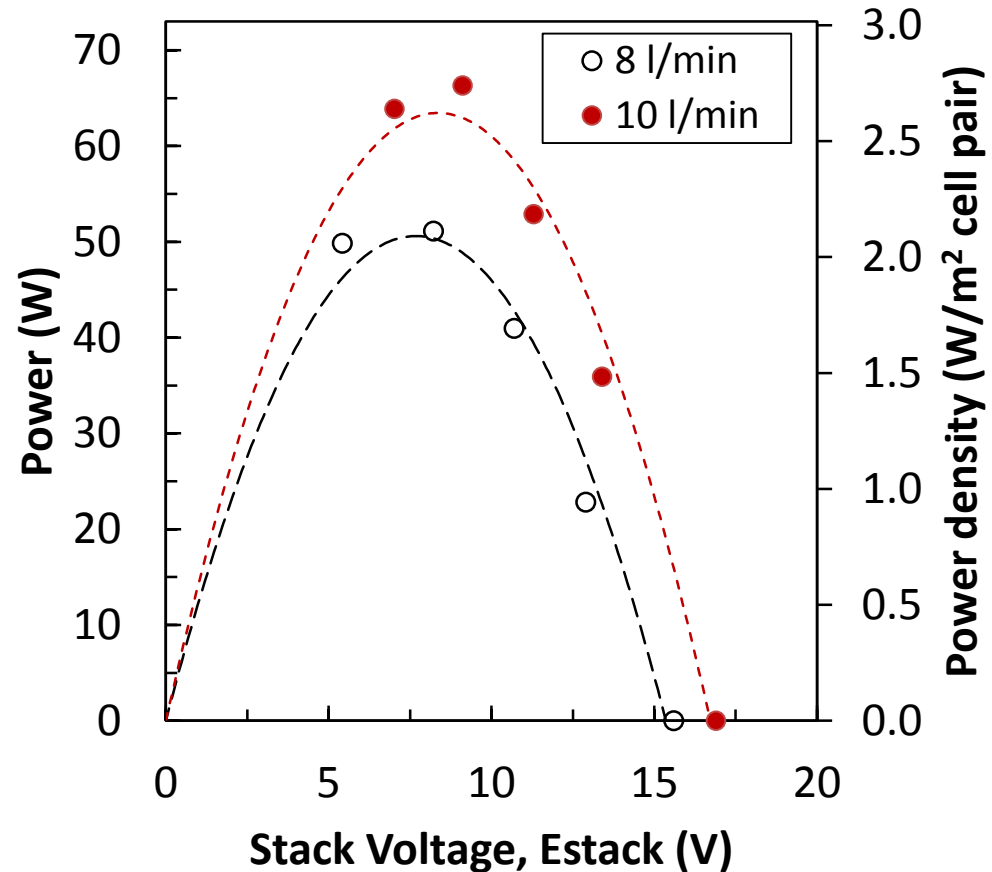




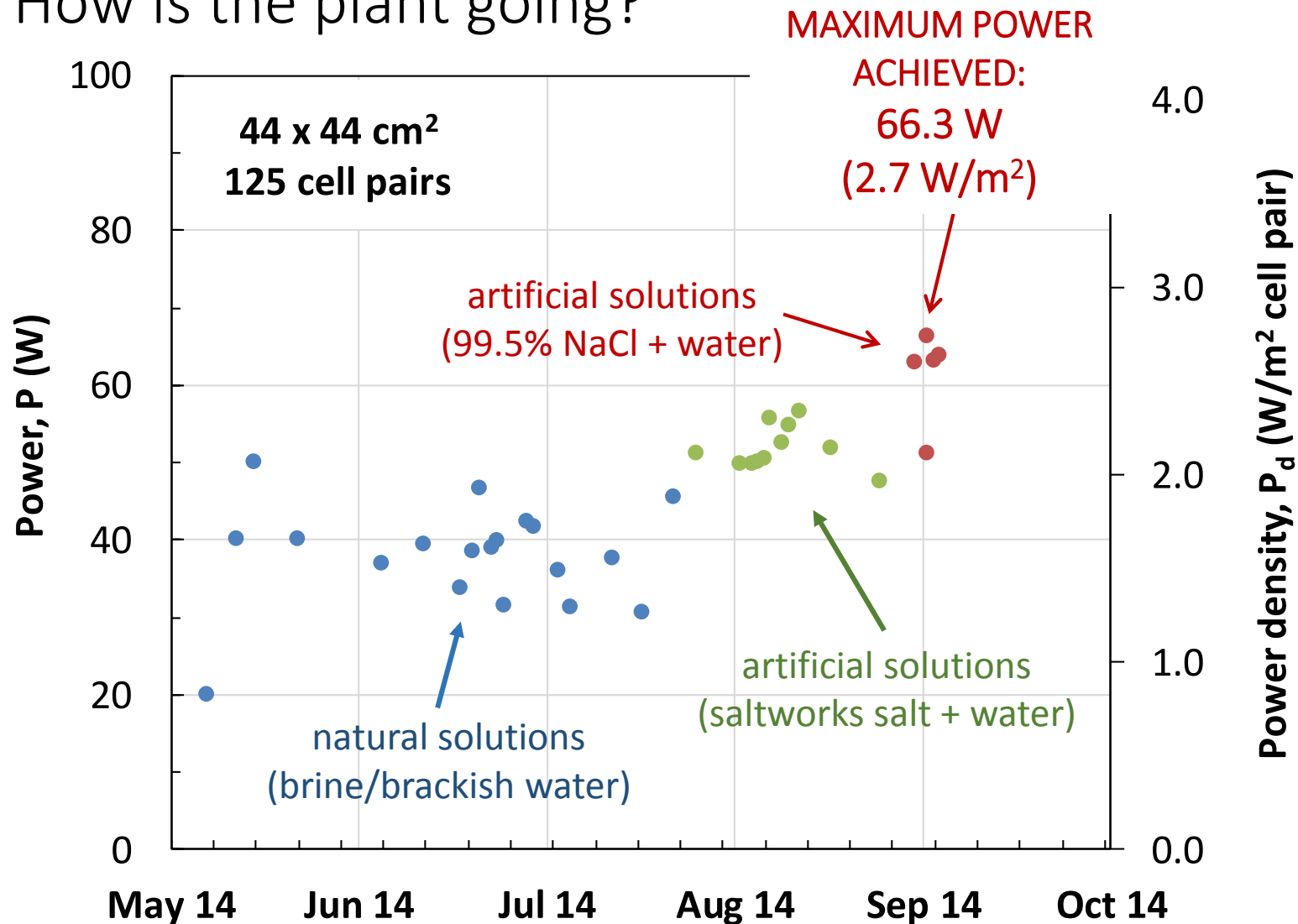
# Power measurements with **artificial** solutions (3/3)

## Influence of dilute flow rate

artificial solutions  
(99.5% NaCl + water)



# How is the plant going?



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Range of variable conditions: brine conductivity: **137 - 230 mS/cm**, dilute conductivity: **0.7 - 7 mS/cm**, temperature: **25-30°C**, flow rates: **8 – 16 l/min**.

M. Tedesco, Performance of the first RED plant operating with natural brackish water and brine  
- SGE Conference 2014

# What's next?

- testing with **large prototypes** (44 x 44 cm<sup>2</sup>, 500 cell pairs)
- **Performance analysis** of the two large prototypes
- Operation with **full plant capacity** (1 module 125 cell pairs + 2 modules 500 cell pairs) using different **plant layouts** (serial/parallel arrangement)
- Investigating the influence of **natural solutions** on long-term performance



# Conclusions

- ✓ A **RED plant with 3 modules** (218 m<sup>2</sup> total cell pairs area) has been **successfully installed** and is currently **under investigation**
- ✓ **No performance loss** after 4 months testing
- ✓ Main achievements so far:
  - using **natural** solutions: **55 W** power output, **2.3 W/m<sup>2</sup>** power density
  - using **artificial** solutions: **66 W** power output, **2.7 W/m<sup>2</sup>** power density
- ✓ **300 W** already measured with each large prototype, with further **testing ongoing...**



# Acknowledgments



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**REAPower**



**EuroMed 2015**

**Desalination for  
Clean Water and Energy  
Palermo, Italy  
10-14 May 2015**



***Thank you  
for your attention***

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